

Amendments to the Claims:

This listing of claims will replace all prior versions and listings of claims in the application:

Listing of Claims:

Claims 1-24 (cancelled)

25. (currently amended) A Microcrystalline microcrystalline paraffin, prepared by a β -zeolite based catalytic hydroisomerization of hydroisomerizing FT (Fischer-Tropsch) paraffins having a carbon chain length distribution in the range from 20 to 105, at temperatures above 200°C, by processing the FT paraffins with a catalyst based on a beta zeolite, the catalyst comprising 60 to 95 by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8 by mass of gamma-aluminum oxide having a specific surface area of 150-350 m²/g, calculated as Al₂O₃ and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of 0.2 to 2.0 by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

26. (currently amended) The Microcrystalline microcrystalline paraffin according to claim 25, wherein, at 25°C the paraffin is not liquid but at least paste-like to solid with a needle penetration value of less than 100 x 10⁻¹ mm, measured in accordance with DIN 51579.

27. (currently amended) The Microcrystalline microcrystalline paraffin according to claim 25, wherein the paraffin is free of aromatic and heterocyclic compounds.

28. (currently amended) The Microcrystalline microcrystalline paraffin according to claim 25, wherein the paraffin is free of naphthenes.

29. (currently amended) The Microcrystalline microcrystalline paraffin according to claim 25, having a proportion by weight of isoalkanes that is greater than that of n-alkanes in the paraffin.

30. (cancelled)

31. (currently amended) Process for preparing a microcrystalline paraffin according to claim 25, by catalytic hydroisomerization by steps of: comprising

A. use of processing FT (Fischer-Tropsch) paraffins, as a starting material, having carbon atoms in the range from 20 to 105; and

B. use of in the presence of a catalyst based on a β-zeolite;

C. use of a process temperature above 200°C; and wherein the process is conducted at a temperature above 200°C, and

D. action of pressure at a pressure in a range of 2 to 20 MPa in the presence of hydrogen; wherein the catalyst comprises 60 to 95 by mass of zeolite of the beta type, based on the combination of all components fired at 800°C, 5 to 39.8 by mass of gamma-aluminum oxide having a specific surface area of 150-350 m²/g, calculated as Al₂O₃ and based on the combination of all components fired at 800°C, and one or more metals of transition group 8 of the periodic table, in an amount of 0.2 to 2.0 by mass, based on the combination of all components fired at 800°C, the one or more transition group 8 metals being attached to the gamma-aluminum oxide.

32. (currently amended) Process according to claim 31, wherein the β-zeolite, has further comprises pores comprising a pore size between 0.50 and 0.80 nm as support material and a metal of transition group 8 as active component.

33. (cancelled)

34. (cancelled)

35. (cancelled)

36. (currently amended) Process according to claim [[33,]] 31, wherein the pressure is 3 to 8 Mpa.

37. (currently amended) Process according to claim [[33,]] 31, wherein the elevated temperature is a process is conducted at a temperature of 230 to 270°C.

38. (currently amended) Process according to claim 31, comprising a step of feeding wherein the hydrogen is fed to the paraffin, characterized by in a feed ratio of hydrogen to FT paraffin from 100:1 to 2000:1 standard m³ per m³.

39. (currently amended) Process according to claim 31, comprising a step of feeding wherein the hydrogen is fed to the paraffin, characterized by in a feed ratio of hydrogen to FT paraffin from 250:1 to 600:1 standard m³ per m³.

40. (previously presented) Process according to claim 31, wherein the process is carried out at a loading from 0.1 to 2.0 v/vh.

41. (currently amended) Process according to claim [[33,]] 32, wherein the catalyst has a pore size between 0.55 to 0.76 nm.

42. (cancelled)

43. (currently amended) Process according to claim [[42,]] 31, wherein the catalyst one or more metals of transition group 8 of the Periodic Table comprises platinum as hydrogenation metal.

44. (previously presented) Process according to claim 43, wherein the platinum content of the catalyst is 0.1 to 2.0% by mass, based on a catalyst fired at 800°C.

45. (currently amended) Process according to claim 31, wherein the FT paraffins have a solidification point range ranging from 70 to 105°C.

46. (currently amended) Process according to claim 31, wherein the microcrystalline paraffins are paraffin is prepared from the FT paraffins in a single process step, optionally additionally with removal of the short chain constituents.

Claims 47-50 (cancelled)

51. (previously presented) Process according claim 31, wherein the process is carried out at a loading from 0.2 to 0.8 v/vh.

52. (previously presented) Process according to claim 43, wherein the platinum content of the catalyst is 0.4 to 1.0% by mass, based on a catalyst fired at 800°C.

53. (previously presented) Process according to claim 45, wherein the FT paraffins have solidification points of 70, 80, 95 or 105°C.

54. (new) Process according to claim 46, wherein the microcrystalline paraffins are prepared from the FT paraffins in a single process step, with removal of the short chain constituents.